## **TECHNICAL INFORMATION**

# THE INFLOW OF UNWANTED AIR CONTROL VALVES CAN HELP SOLVE THE PROBLEM

### AIR IN PRESSURIZED PIPES

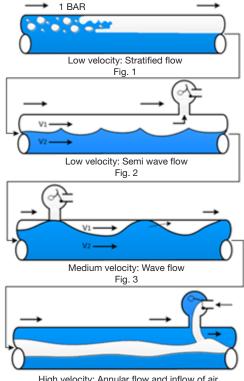
The main reason for the inflow of air in public water distribution systems is excessive water velocity. Air traveling with water in pressurized pipes can result in high turbulence derived from the dynamic characteristics of each element (compressibility and gravity).

How can high velocity prevent the extraction of air and increase the inflow of air? In order to understand this in a simplified way Fig. 1 to 4 show how air is flowing in the pipe.

In Fig. 1 and 2 water is flowing at an acceptable velocity of maximum 2 m/s. At this velocity extraction of air with automatic air valves is easy.

Fig. 3 shows an increase in velocity of air (air vents open) compared with water velocity. Waves will be formed and extraction of air is more difficult.

At high velocities (Fig. 4) the water tends to have an annular flow. In these cases, extraction of air is impossible and air valve action will be inverted with the inflow of a large volume of air inside the pipeline.



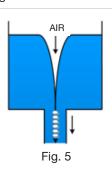
High velocity: Annular flow and inflow of air Fig. 4

### VELOCITY AND INFLOW OF AIR

Large volume of air can be introduced in the pipe system as in the following examples: Fig. 5 and 6 - Vortex in reduced volume head loss tanks Fig. 7 - Vortex in a pumping station with reduced tank volume



Vortex



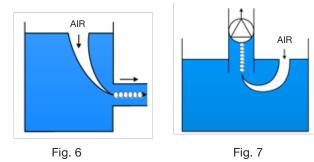
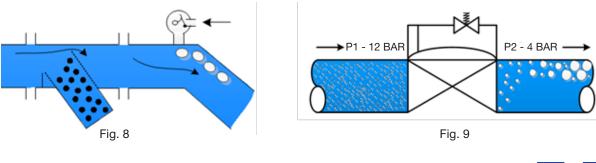


Fig. 8 - Clogged protection filter or a partially closed valve in the system Fig. 9 - Micrometric cells of dissolved air will grow in a pressure reducing station

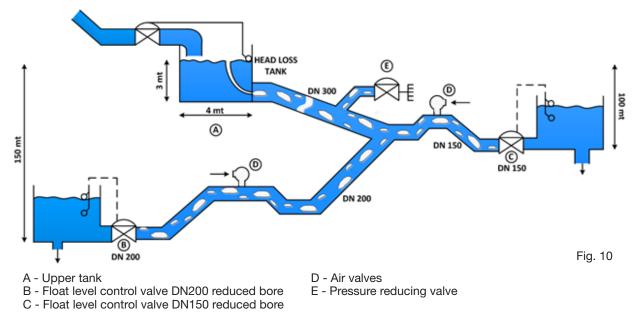




CONTROL VALVES CAN HELP SOLVE THE PROBLEM

### WATER DISTRIBUTION SYSTEM - INCORRECTLY SIZED

Fig. 10 shows an example of a water distribution system with incorrectly sized on/off level control valves in head loss tanks.



Presence of a large volume of air in the system will cause damaging waves and malfunction of the control valves (seat chatter, vibration and water hammer).

Example: Valve B - DN200 Reduced bore on/off float level Inlet pressure: 10 bar Valve C - DN150 Reduced bore on/off float level Inlet pressure: 15 bar

#### K<sub>v</sub> values per DN

	DN									
Model	50	65	80	100	125	150	200	250	300	
Reduced bore (standard)	NA	53	83	119	135	202	435	734	990	
Full bore (optional)	44	76	116	175	NA	400	710	947	1355	

K<sub>v</sub>: Cubic meters of water at 18°C flowing through the open value in one hour with  $\Delta P = 1$  bar

B:	DN200	reduced	bore	$K_v =$	435
-					

C: DN150 reduced bore  $K_v = 202$ 

Maximum flow fully open value  $Q = K_v \sqrt{\Delta P}$ B: 1683 m<sup>3</sup>/h C: 639 m<sup>3</sup>/h

Velocity in the pipeline when the valves B and C are fully open:

 $V = \frac{354 \cdot Q}{DN^2}$  DN300: 9 m/s DN200: 15 m/s DN150: 10 m/s

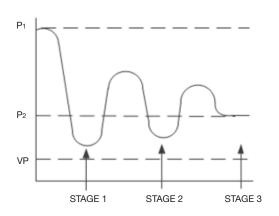
At this velocity, a vortex will certainly be produced in the upper tank (A) with a large volume of air inflow. Air valves (D) do not work due to annular flow, and inflow of air will occur due to the Venturi effect.

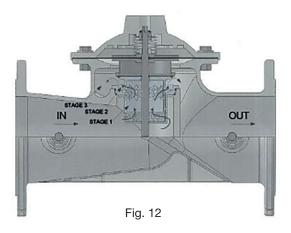


# CONTROL VALVES CAN HELP SOLVE THE PROBLEM

### HOW TO SOLVE THE PROBLEM OF SYSTEM COLLAPSE

 Correctly sized valves with anti-cavitation trim to limit the maximum velocity to 2m/s: Valve size DN80 full bore (Example: Valve C in the system shown in
Fig. 10)



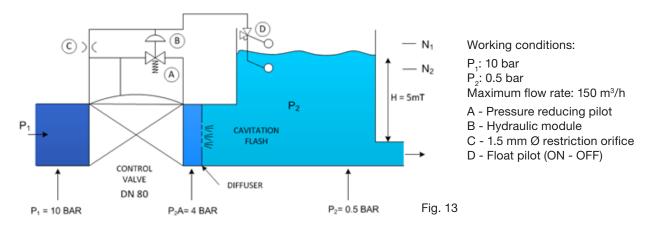


#### A combined 3-phase operation

When the valve starts to open, flow converges in the seat cage. The slide plug cylinder opens the perforated slots on the seat cage at the same time as slots with large areas open in the upper part of the slide plug cylinder upstream of the seat. The flow converges on the center of the cylinders and the slots act as a flow divider allowing potential cavitation to dissipate in this first stage.

The upper slots of the sliding cylinder will then again divide the flow and dissipate energy in a second stage preventing flow jets to stick to the body walls downstream of the seat. In the third stage, bubbles collapse with a minimum energy without any cavitation effect and with low noise.

2) A correctly sized standard valve with a special pilot system and a correctly sized diffuser to limit the maximum velocity to 2 m/s: Valve size DN80 reduced bore (Example: Valve C in the system shown in Fig. 10)



When the  $N_2$  level is reached, hydraulic module (B) opens pilot (A).

The main valve reduces the pressure to a stable value of 4 bar upstream of the diffuser (pressure reducing pilot set to 4 bar), preventing cavitation inside the valve.

When the  $\mathrm{N_1}$  level is reached, hydraulic module (B) closes the main valve.

To increase the maximum flow rate, increase the set pressure of the pilot (B).

To decrease the maximum flow rate, decrease the set pressure of the pilot (B) but maintain the cavitation free values.

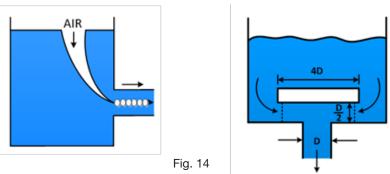


# CONTROL VALVES CAN HELP SOLVE THE PROBLEM

#### **VORTICES - PREVENTION**

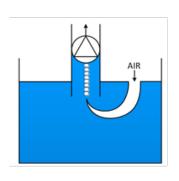
Even at low flow demand, vortices can occur in small volume head loss tanks and pumping stations.

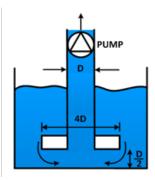
INFLOW OF AIR IN HEAD LOSS TANKS



#### INFLOW OF AIR IN PUMP STATIONS

The inflow of air caused by the formation of a vortex in a pumping station can be very harmful. Air is a compressible fluid and if the pump stops due to power failure, the risk of water hammer intensity will be increased with the presence of air. High surges will be violent and destructive.





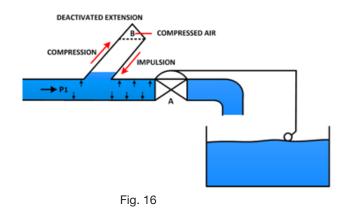
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Fig. 15

#### **RUPTURES CAUSED BY PERMANENT AIR POCKETS**

Air is an element that may cause structured damage in an installation. In a branch, pipe extensions not in use can work as a pneumatic piston creating increasing and decreasing successive pressure surges causing material fatigue.

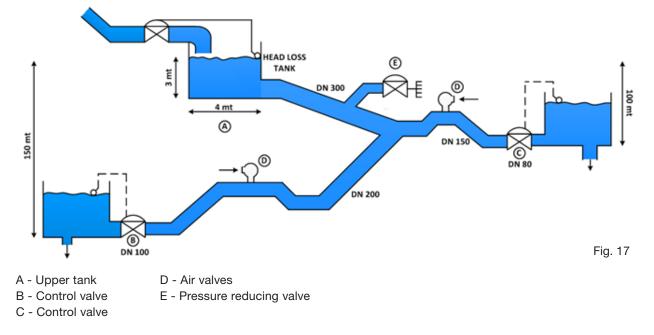
At sudden closure of a control valve in a system,  $P_1$  increases compressing the air and absorbing the inherent energy immediately after the compression. The air under pressure acts as a pneumatic cylinder, causing successive hydraulic waves that cause damage in the system structure.





CONTROL VALVES CAN HELP SOLVE THE PROBLEM





#### CORRECT CHOICE OF VALVES

Modulating float level instead of ON/OFF control valves.

VALVE C: DN80 full bore with anti-cavitation trim to limit velocity at maximum flow (Fig. 12) or:

DN80 reduced bore standard valve with a correctly sized diffuser to limit velocity and maximum flow (Fig. 13)

VALVE B: Same as valve C but DN100

Both valves have a pressure sustaining function to prevent inlet pressure failure on pressure reducing valve E to ensure system stability (Fig. 18).

The maximum velocity in the system is 2 m/s



Fig. 18 Modulating float/ Pressure sustaining

